

The background features a large, faint, circular watermark of the United States Environmental Protection Agency (EPA) seal. The seal includes the text "UNITED STATES" at the top and "ENVIRONMENTAL PROTECTION AGENCY" around the bottom. In the center is a stylized flower with a sun-like center.

# Demand Management and Process Optimization for WWTPs

Brendan Held, EPA Region 4

KY EEC Demand Management Conference

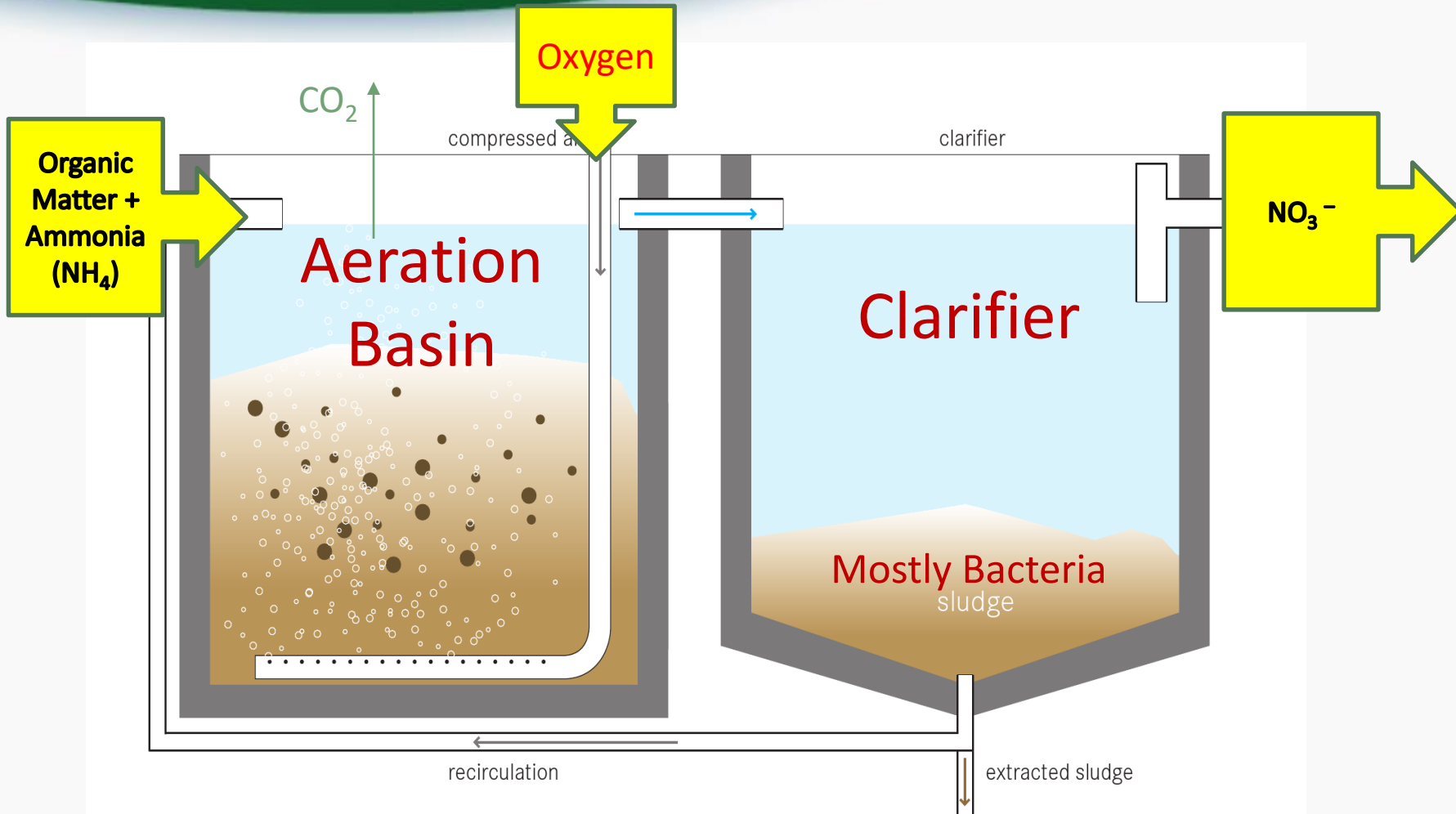
March 22, 2018

# Overview

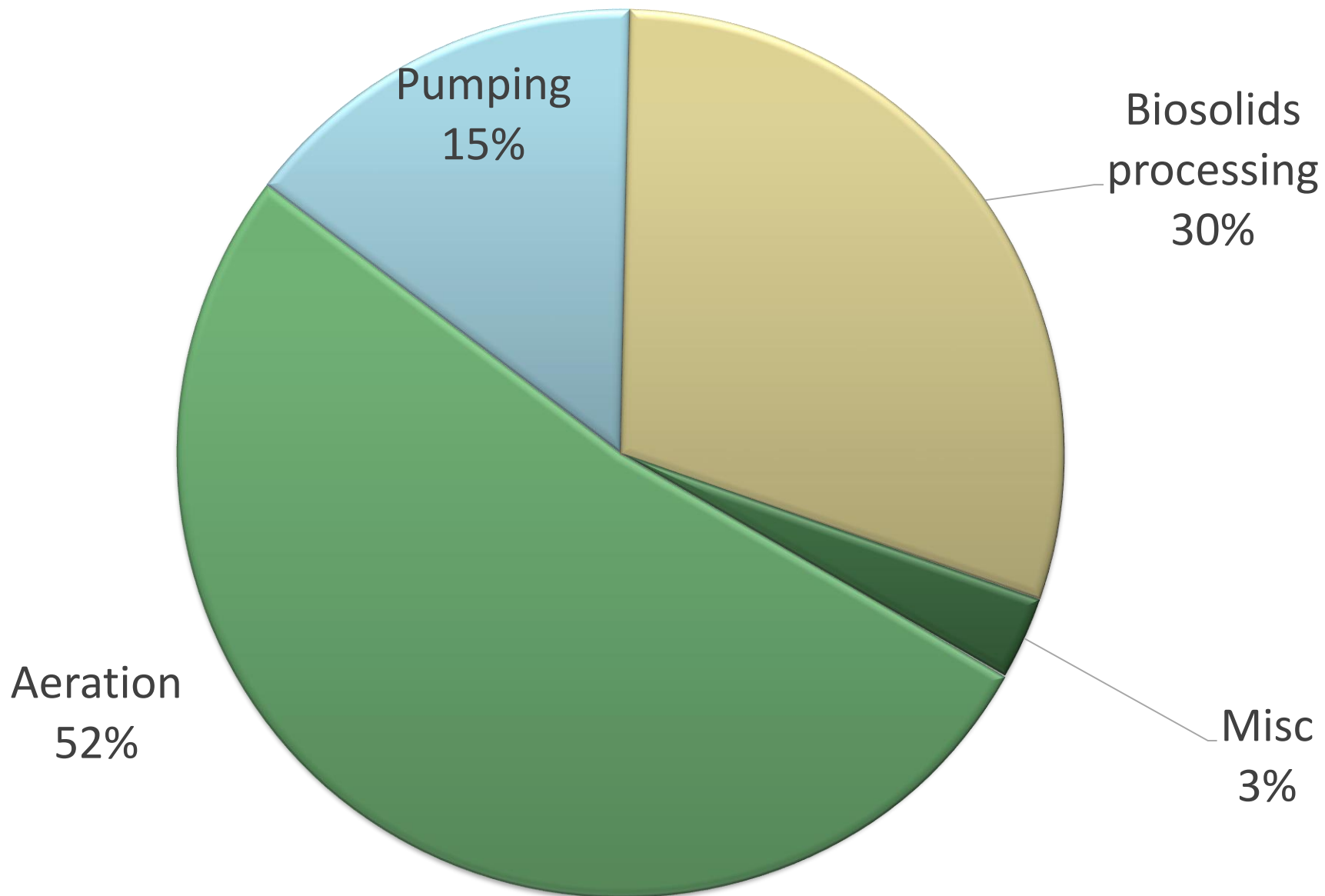
- Wastewater basics and the activated sludge process
- Energy use at WWTPs
- Demand Management Strategies at WWTPs
- Demand Management Strategies at WTPs
- Case Studies
- Resources

# Activated Sludge Process

It's a bacteria farm!

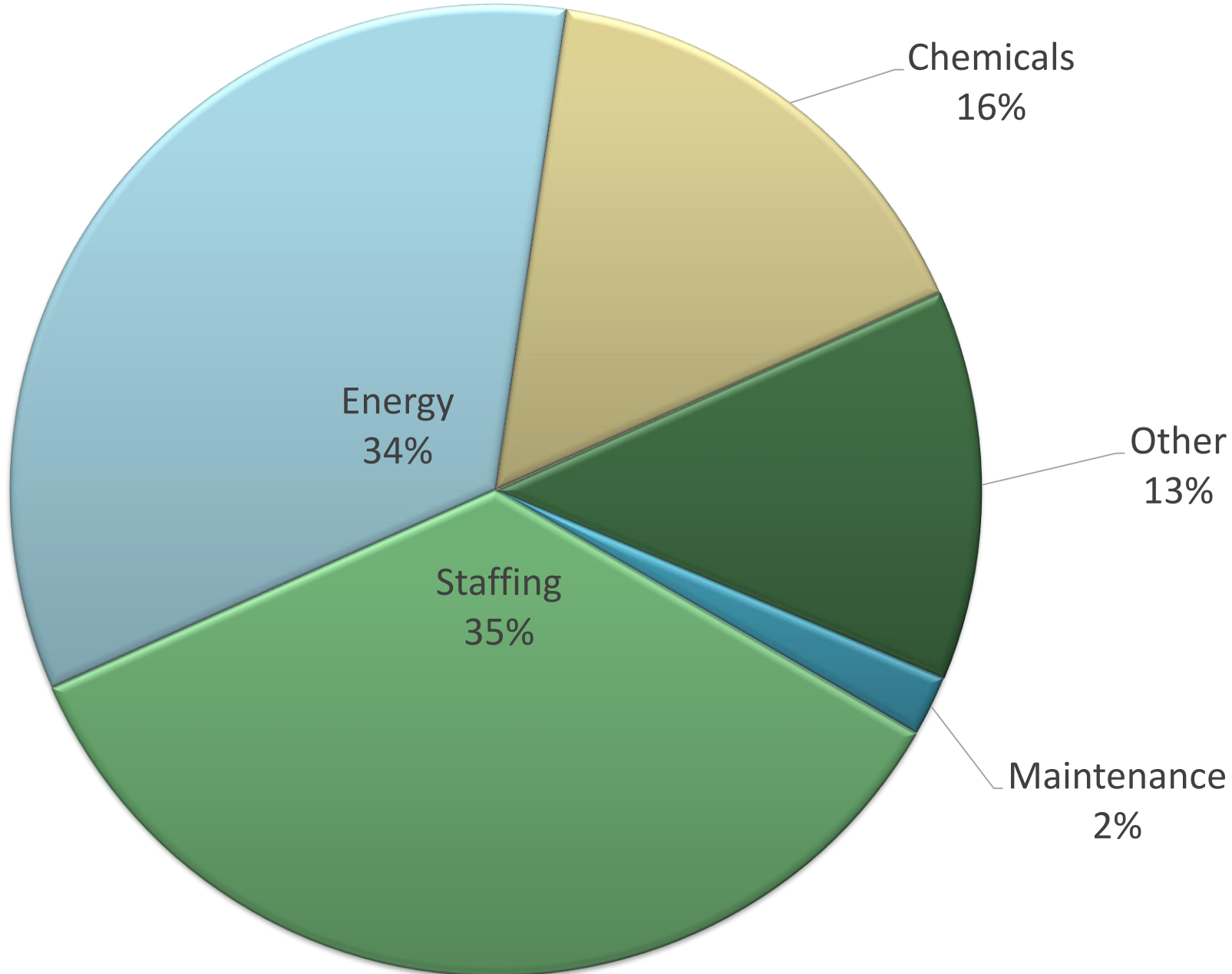


# Typical Energy Use at WWTPs



Source: Hazen and Sawyer

# Typical Operating Costs at Public Water Systems




# Recognizing the Opportunity

## Excess by design:

- 20 year design life means excess capacity for most of a plant's service.
- Some growth forecasts are based on the premise that excess capacity will lure industry.
- Operations manuals recommend a conservative 2.0 mg/L dissolved oxygen concentration at all times.

## Excess by habit:

- If equipment is available, it tends to get used. (See first point.)
- If 2.0 mg/L of dissolved oxygen is good, 3.0 must be better. (It isn't.)
- Who sees the savings? Operators rarely see bills. (And worry about budget cuts if savings are too effective.)



# Demand Management Strategies at WWTPs

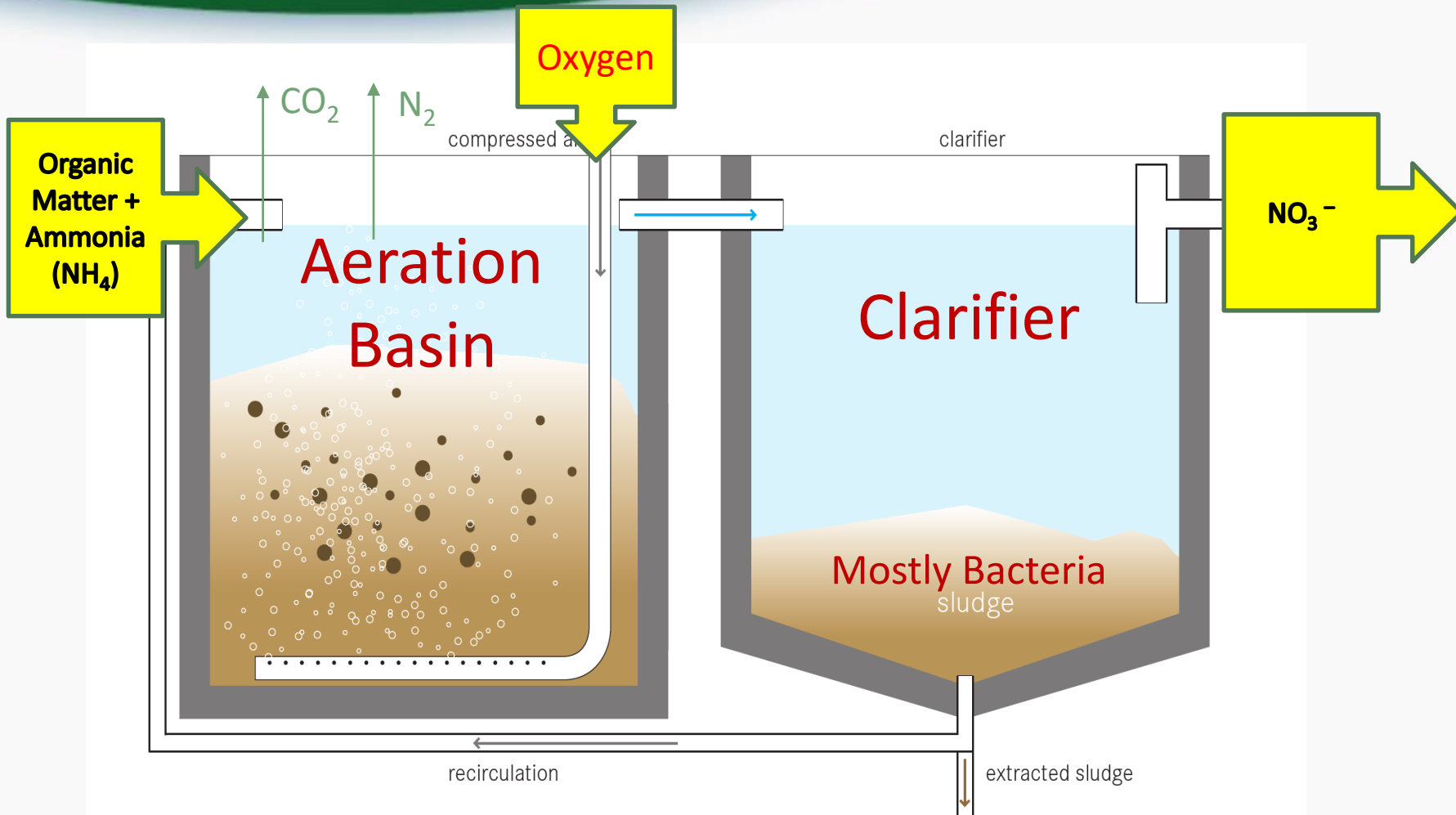
# Strategies for Reducing Aeration

- Reduce aerator runtimes, and/or number of aerators in service
- VFDs and improved SCADA can help ensure a proper DO setpoint
- BioTiger, an Excel-based model developed through cooperation of DOE, EPA and University of Memphis (More on this under Resources.)



# Intermittent Aeration

It's a bacteria farm!



# Intermittent aeration

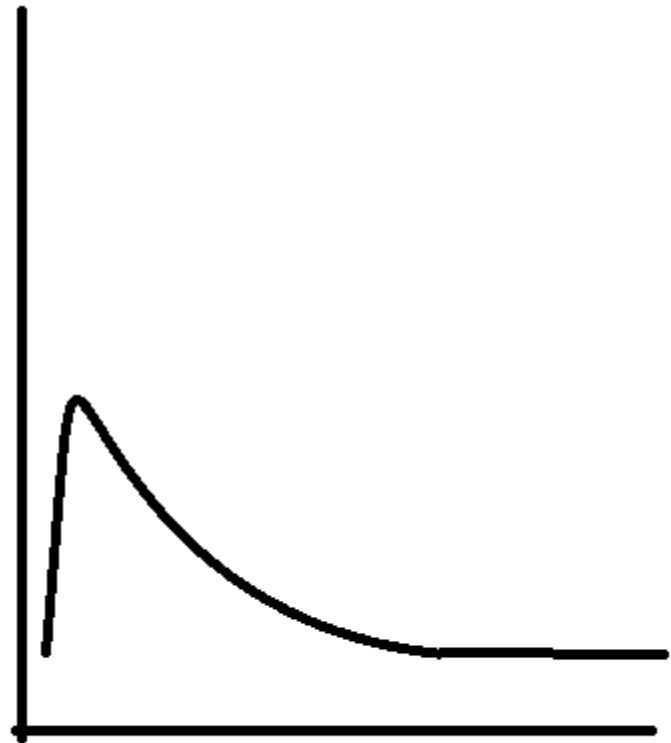
- Nitrogen enters the WWTP as ammonia and organic nitrogen, such as urea
- Slow growing AOBs use supplied oxygen to convert those forms to nitrite ( $\text{NO}_2$ ) and nitrate ( $\text{NO}_3$ )
  - This also consumes alkalinity. This is ok to a degree, but if alkalinity runs out, the system could become acidic and impair performance
  - Many facilities do this to meet strict ammonia limit
- Given the right conditions, other bacteria can use nitrite and nitrate in their metabolic process
  - These conditions include a low oxygen environment, which can be created when aeration is reduced or paused
  - This returns alkalinity to the system and can improve solids settling
  - Many systems do not routinely perform this step unless a limit of Total Nitrogen is imposed

# A word about inrush current

Myth: Frequent starts and stops of large motors will increase my demand

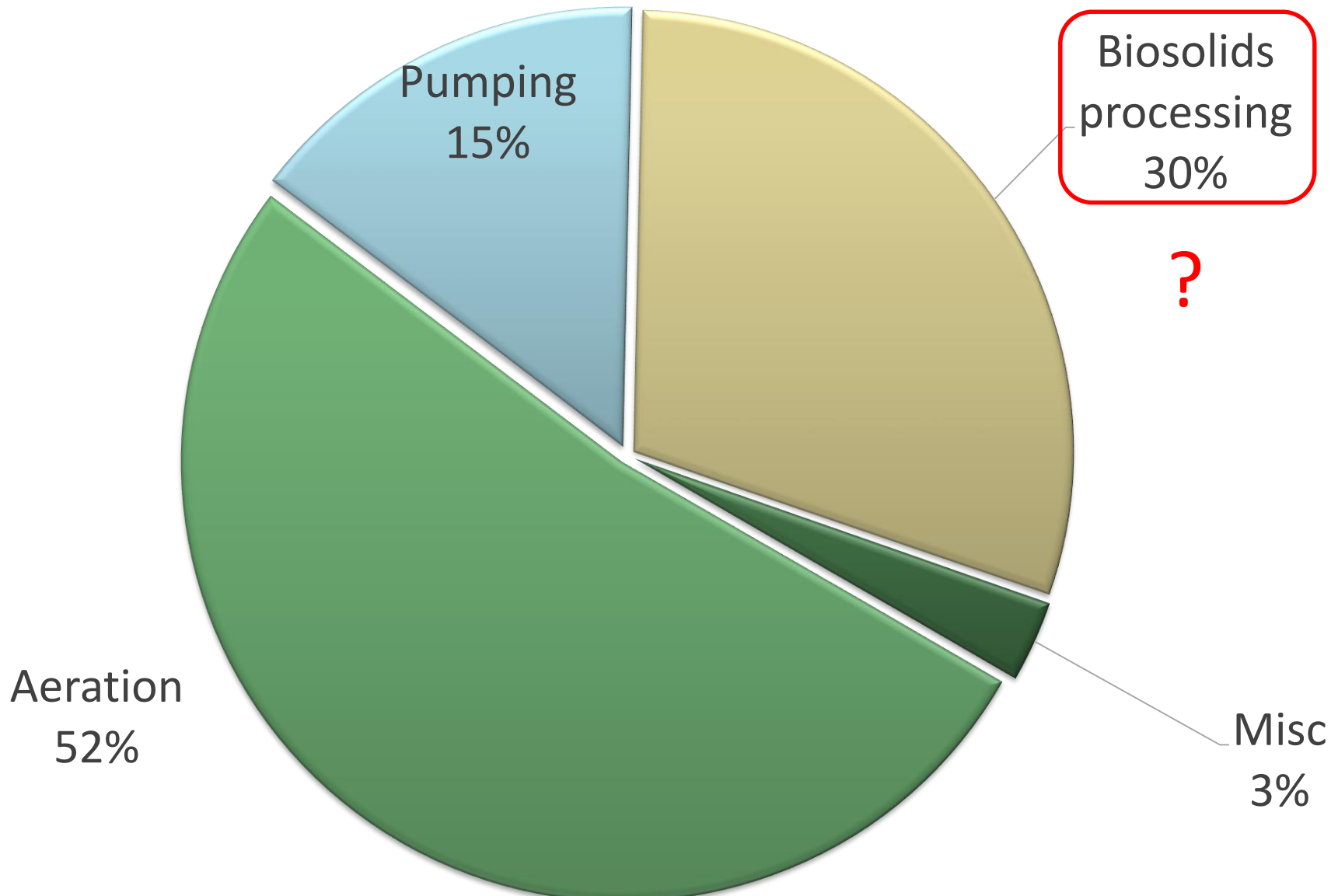
Fact: There is a large spike in kW draw when motors are started (up to 6x “full” power) but the spike only lasts a couple seconds. Over the 15-minute demand window, this amounts to less than 0.2% increase.

Another Fact: This excess current will dissipate in the form of heat, which can accelerate wear. This is where soft starts can help.



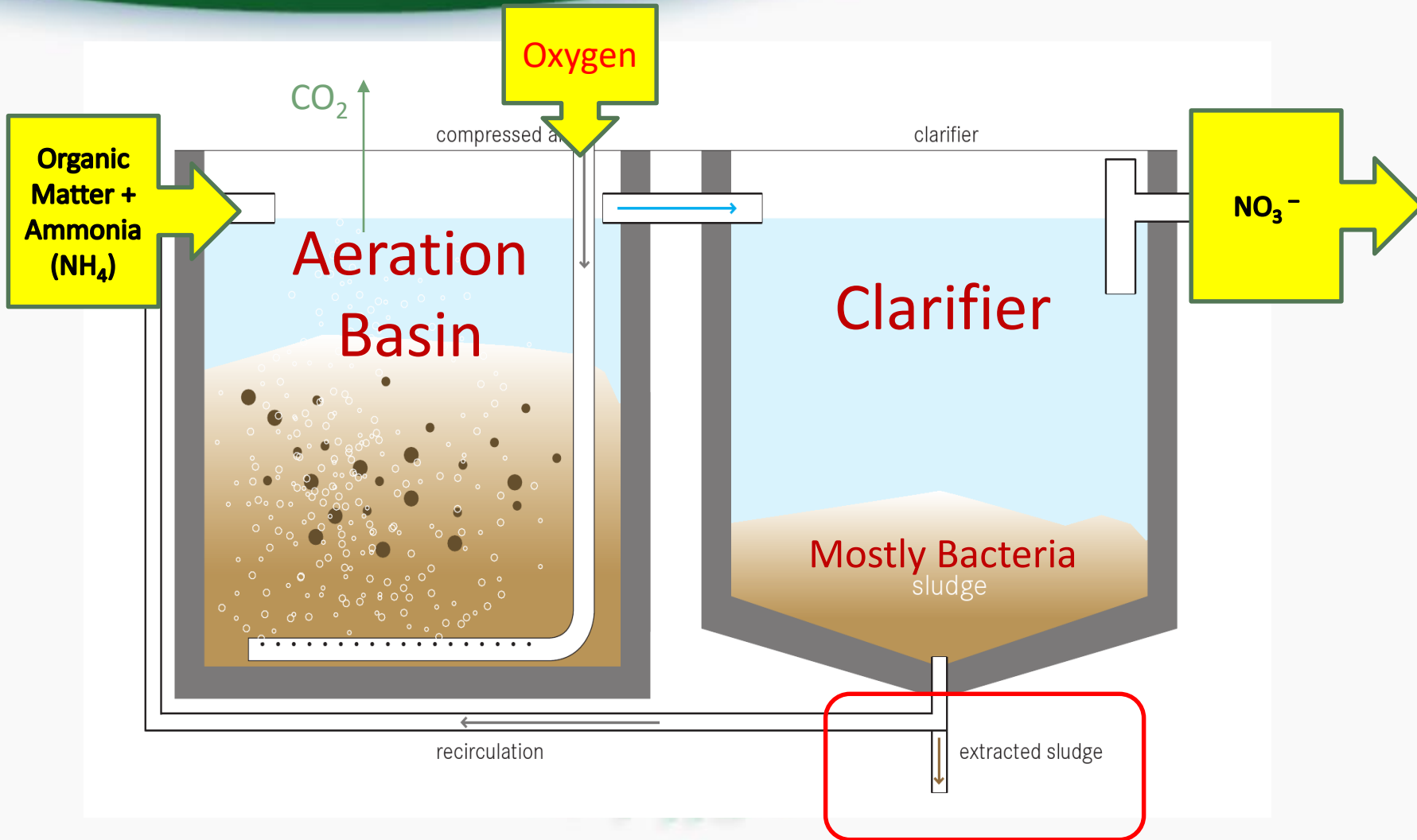
# Strategies for reducing aeration

Typical Energy Use at WWTPs



# Activated Sludge Process

It's a bacteria farm!



# Aerobic Digestion

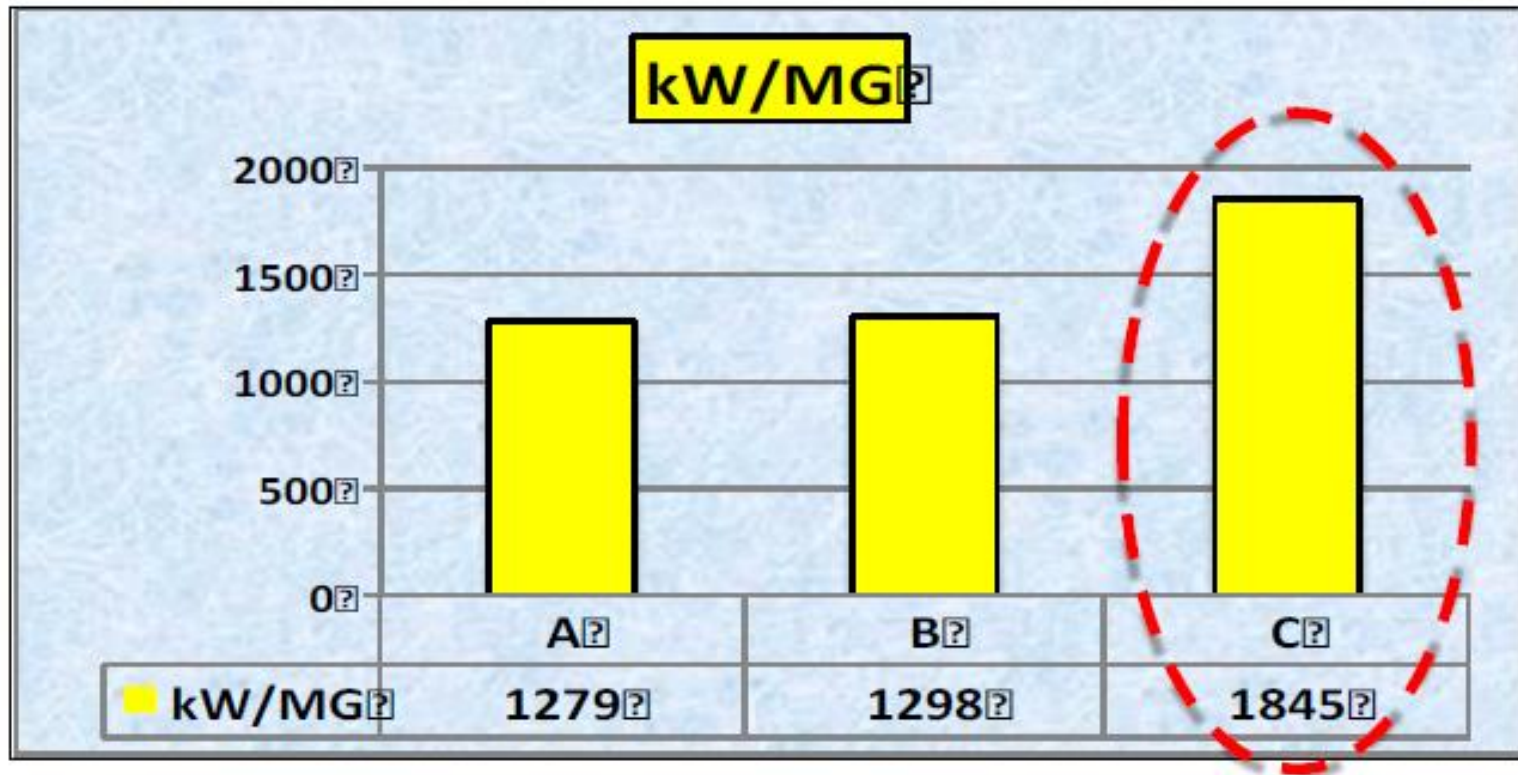
- Waste sludge or biosolids are further processed to reduce the risk of spreading pathogens when they are ultimately disposed.
- Most often this is a process called digestion. Solids are collected and aerated to allow for further destruction of the solids.
- In facilities with excess capacity, biosolids often remain in the activated sludge system much longer than designed.
- Solids are often well digested before they are removed, requiring less aeration and detention time in the digester.
- Using a Specific Oxygen Uptake Rate (SOUR) test to meet vector attraction reduction requirements is preferred to measuring destruction of solids.



# Demand Management at Drinking Water Plants



# Real-world Well Analysis Findings



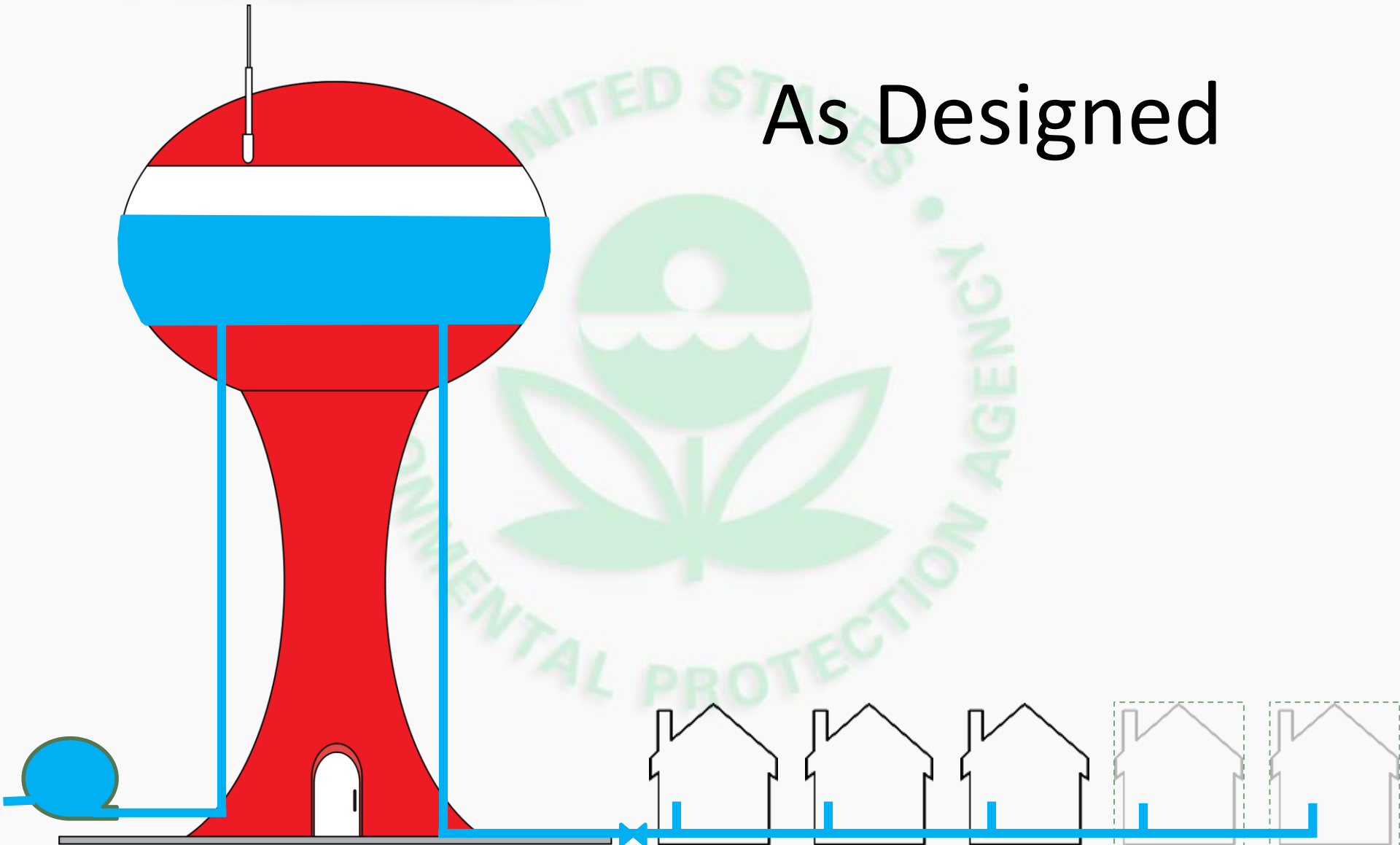
Well C uses 40% more power to do the same amount of work. Just moving some of this load over to another well can save thousands of dollars a year. Actions such as these gain credibility and make it easier to get money for future projects. No tools were required, just looking at the data.





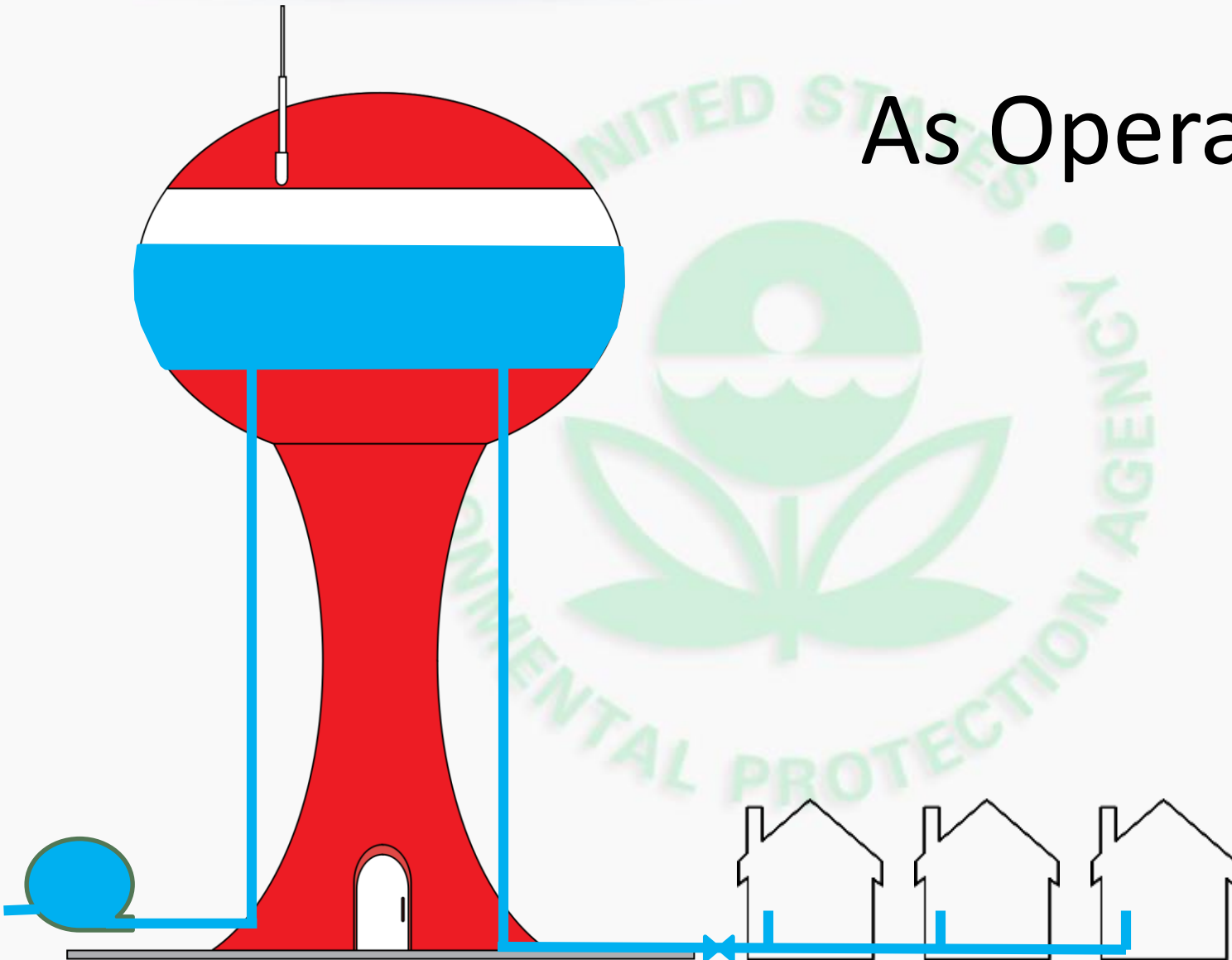
# Elevated Tanks – Top Capacity Level

As Designed



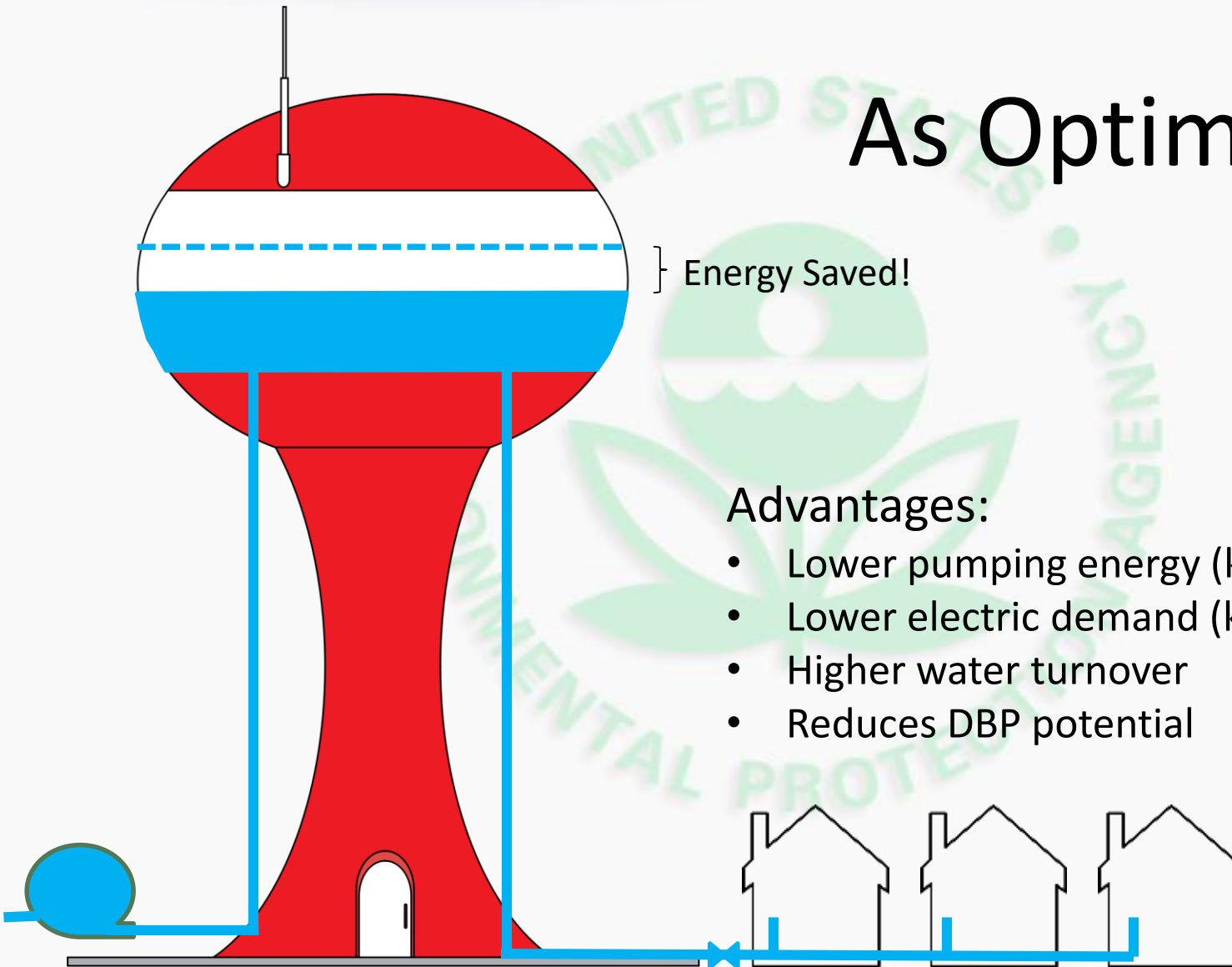
# Elevated Tanks – Top Capacity Level

As Operated



# Elevated Tanks – Top Capacity Level

## As Optimized



### Advantages:

- Lower pumping energy (kWh)
- Lower electric demand (kW)
- Higher water turnover
- Reduces DBP potential

# How are you being charged?



Time of Use Rates?  
Real Time Pricing?



\$ per kWh per kVA??  
Contract Minimums?



Incentive Programs?

# Early Energy Team Objectives

## How are you being charged?

### MONTHLY RATE (SECONDARY)

Base Charge:  
\$50.00 per customer; plus

Demand Charge  
Line Item

Charge for Billing Capacity:  
\$4.74 per kW of billing capacity; plus

Charge for Energy:  
For the first 250 kWh per kW of billing capacity:  
8.9331¢ per kWh for all kWh.  
For all over 250 kWh per kW of billing capacity:  
6.9668¢ per kWh for all kWh.

Ratchet  
effect

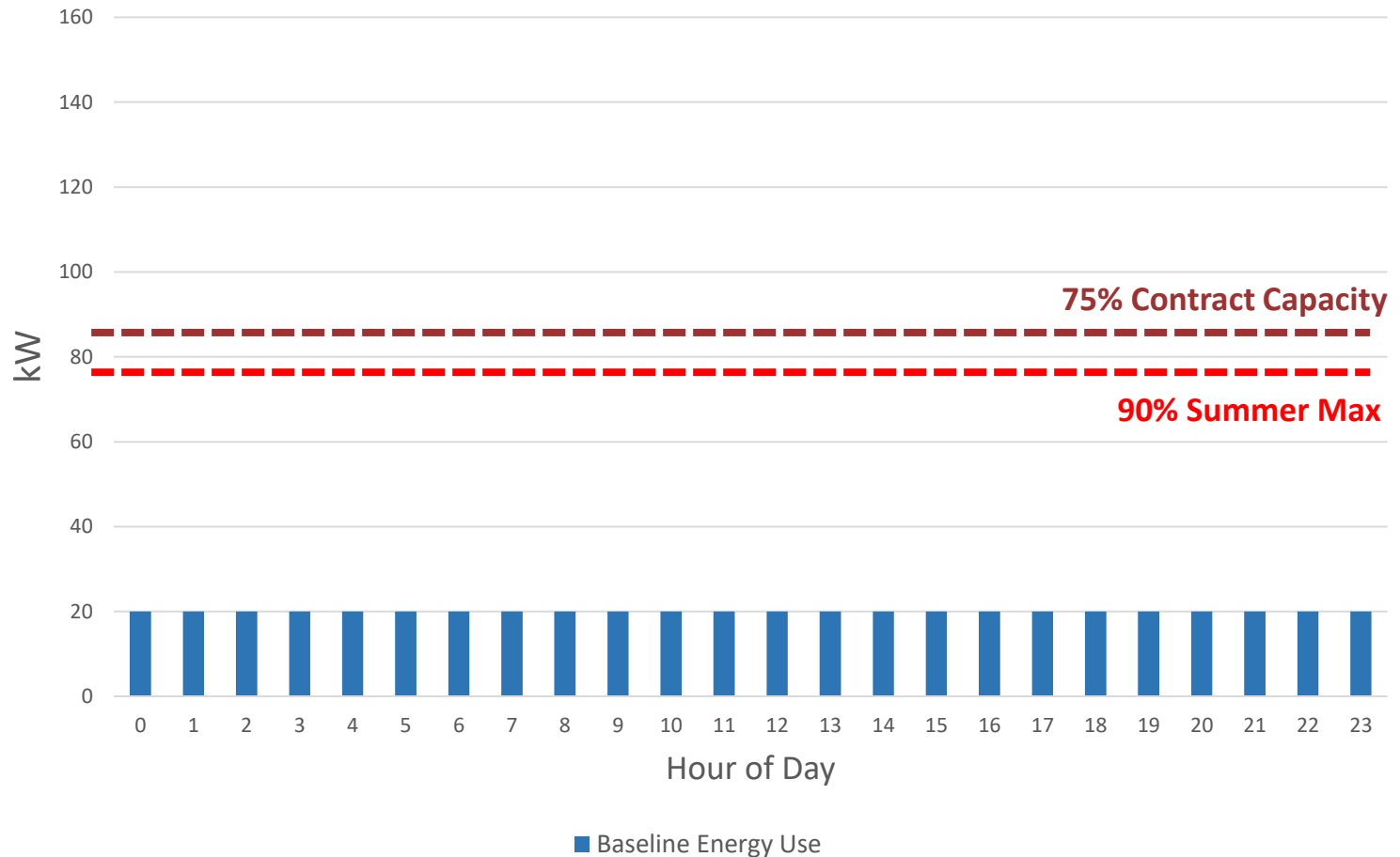
Higher kW  
demand =  
higher kWh  
marginal  
price

### DETERMINATION OF BILLING CAPACITY

The monthly billing capacity shall be the measured maximum integrated fifteen (15) minute capacity during each billing period of approximately thirty (30) days measured in kW; provided, however, that such capacity shall be no less than ninety percent (90%) of the measured maximum capacity requirements established during the billing months of June through September falling within the eleven (11) months preceding the billing period or seventy-five percent (75%) of the contracted capacity, whichever is greater. No billing capacity shall be for less than 5 kW for secondary service from the distribution facilities, 25 kW for primary service, or 100 kW for service from the transmission facilities.

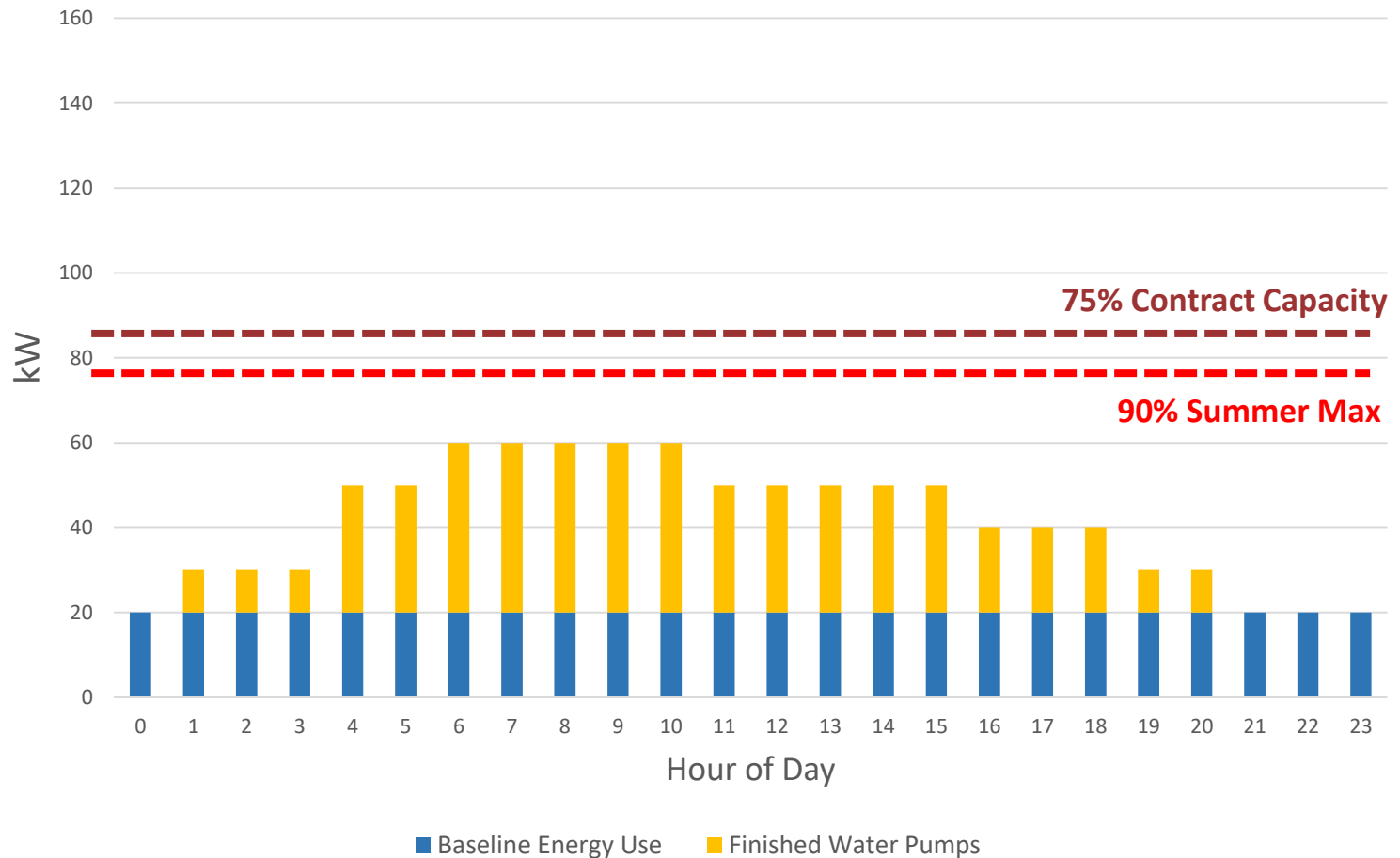
# How are you being billed?

Daily Energy Use Profile



# How are you being billed?

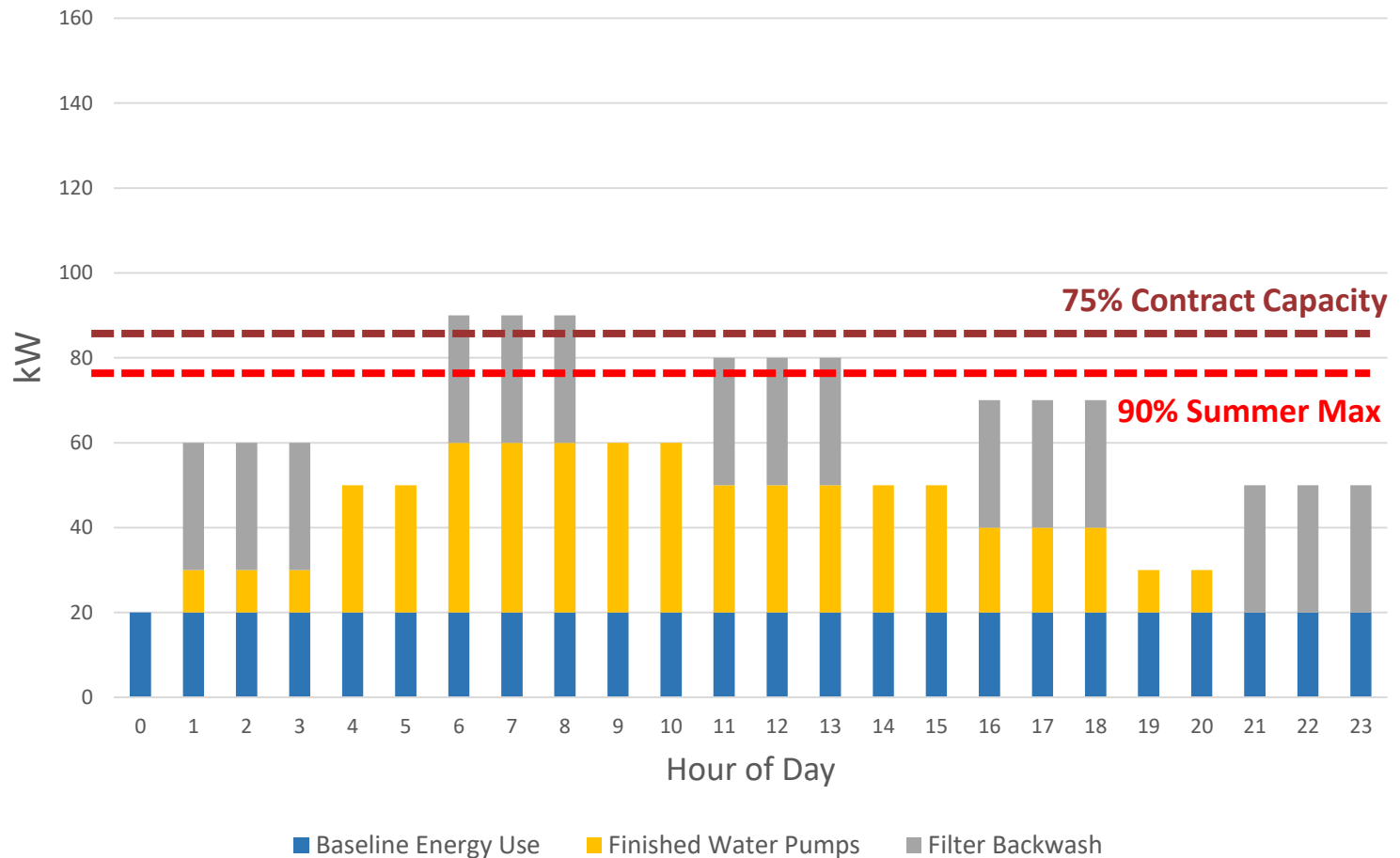
## Daily Energy Use Profile





# How are you being billed?

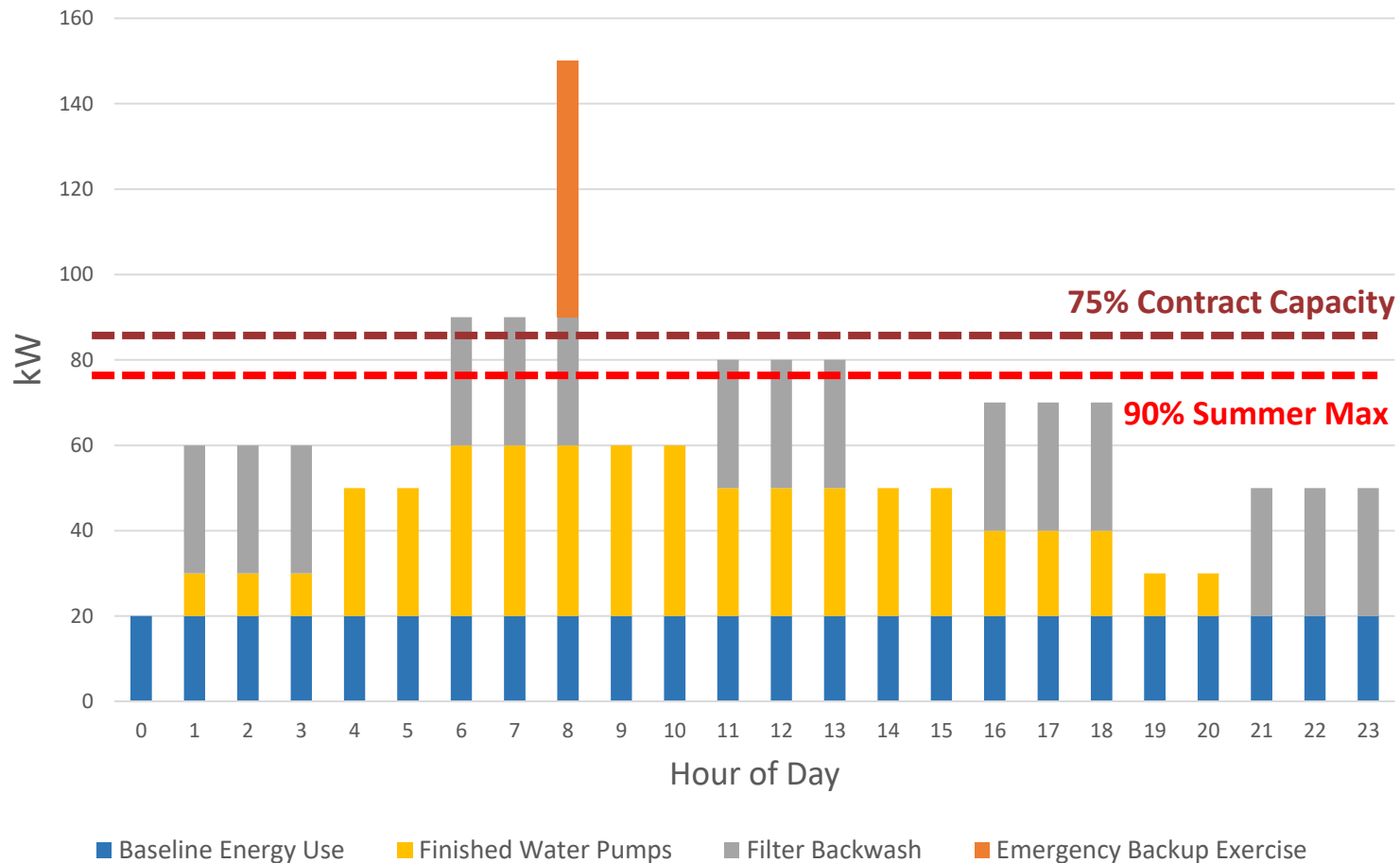
## Daily Energy Use Profile





# How are you being billed?

## Daily Energy Use Profile



# Demand Management

## How are you being charged?

### MONTHLY RATE (SECONDARY)

Base Charge:  
\$50.00 per customer; plus

Charge for Billing Capacity:  
\$4.74 per kW of billing capacity; plus

Charge for Energy:  
For the first 250 kWh per kW of billing capacity:  
8.9331¢ per kWh for all kWh.

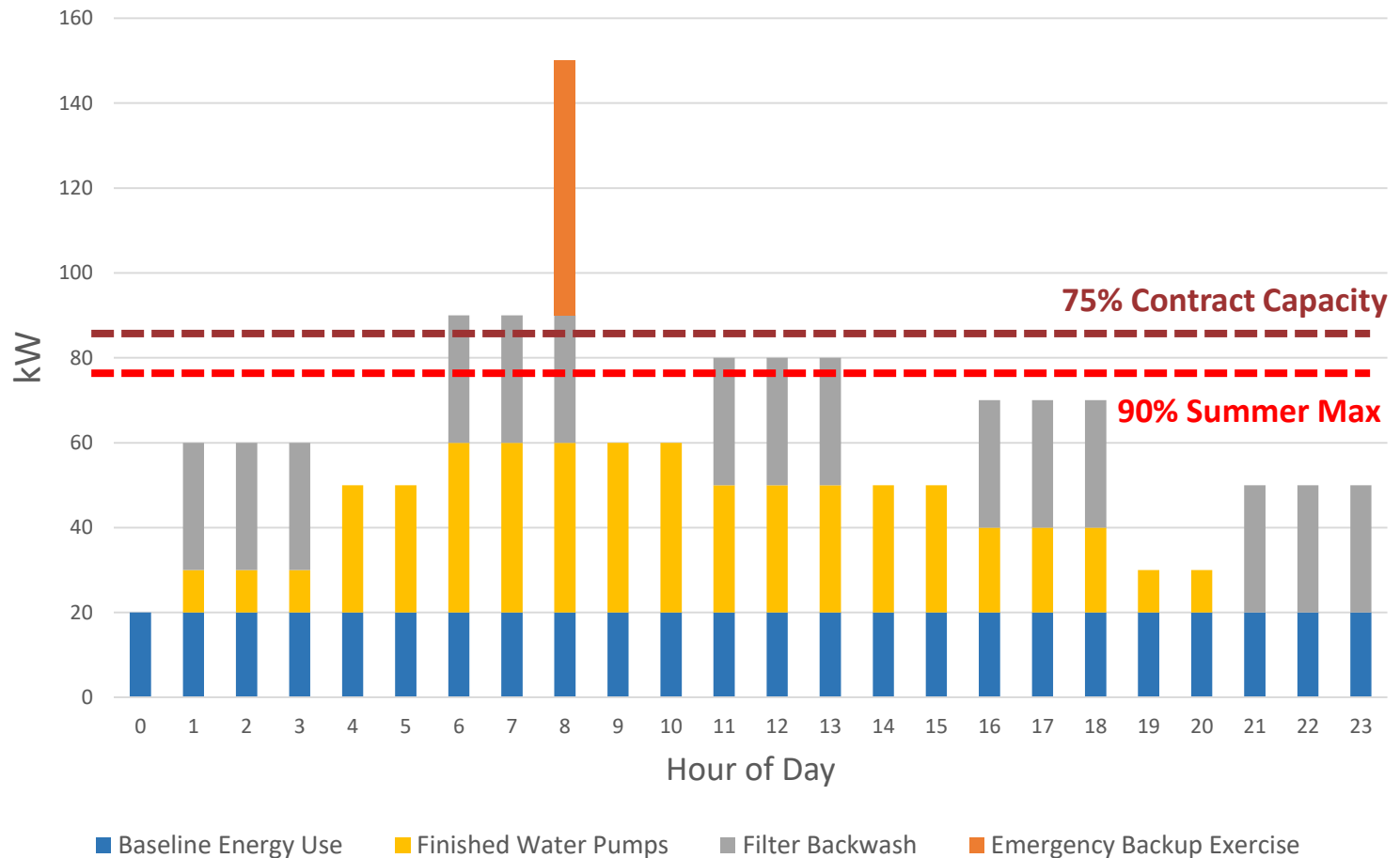
For all over 250 kWh per kW of billing capacity:  
6.9668¢ per kWh for all kWh.

### DETERMINATION OF BILLING CAPACITY

The monthly billing capacity shall be the measured maximum integrated fifteen (15) minute capacity during each billing period of approximately thirty (30) days measured in kW; provided, however, that such capacity shall be no less than ninety percent (90%) of the measured maximum capacity requirements established during the billing months of June through September falling within the eleven (11) months preceding the billing period or seventy-five percent (75%) of the contracted capacity, whichever is greater. No billing capacity shall be for less than 5 kW for secondary service from the distribution facilities, 25 kW for primary service, or 100 kW for service from the transmission facilities.

# Demand Management

## Daily Energy Use Profile

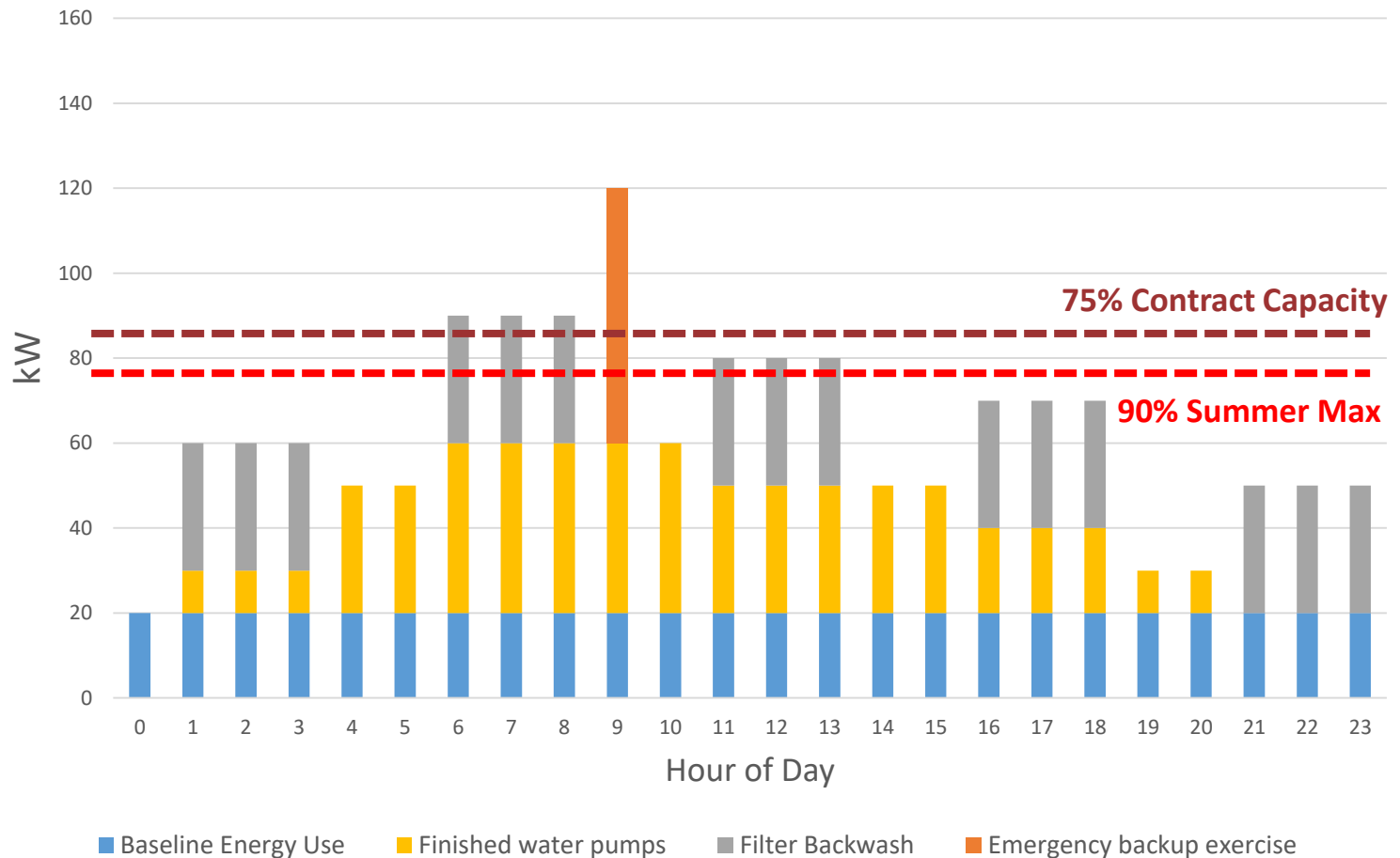


# Demand Management

	Scenario 1
kW billing capacity	150
kWh consumed	45300
kWh/kW	302
Total kW cost	\$711
kWh cost (up to 250 kWh/kW)	\$3350
kWh cost (over 250 kWh/kW)	\$2613
Base charge	\$50
<b>Total Daily Charge</b>	<b>\$6723</b>
<i>% Savings</i>	-
<i>Annual Savings</i>	-

# Demand Management

## Daily Energy Use Profile-Scenario 2

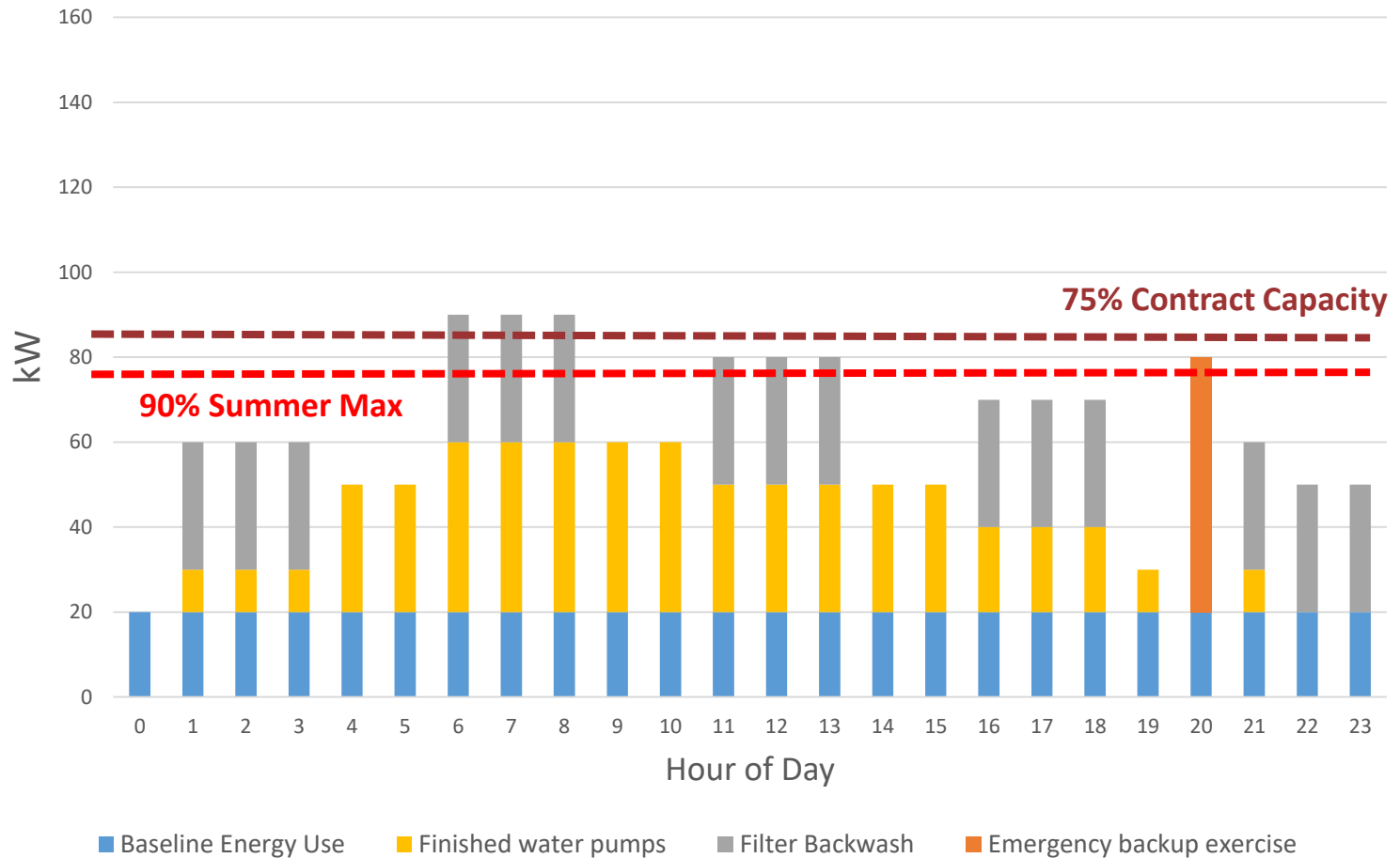


# Demand Management

	Scenario 1	Scenario 2
kW billing capacity	150	120
kWh consumed	45300	45300
kWh/kW	302	378
Total kW cost	\$711	\$569
kWh cost (up to 250 kWh/kW)	\$3350	\$2680
kWh cost (over 250 kWh/kW)	\$2613	\$2090
Base charge	\$50	\$50
<b>Total Charge</b>	<b>\$6723</b>	<b>\$5389</b>
<i>% Savings</i>	-	19.9%

# Demand Management

Full Profile -Scenario 3



# Demand Management

	Scenario 1	Scenario 2	Scenario 3
kW billing capacity	150	120	90
kWh consumed	45300	45300	45300
kWh/kW	302	378	503
Total kW cost	\$711	\$569	\$426
kWh cost (up to 250 kWh/kW)	\$3350	\$2680	\$2010
kWh cost (over 250 kWh/kW)	\$2613	\$2090	\$1567
Base charge	\$50	\$50	\$50
<b>Total Charge</b>	<b>\$6723</b>	<b>\$5389</b>	<b>\$4054</b>
<i>% Savings</i>	-	19.9%	39.7%





# Case Studies



- Each basin had six 75-HP aerators and 2 40-HP mixers running 24/y
- Took one basin and clarifier out of service
- Reduced runtimes of remaining aerators to 18 hrs/d.
- Reduced demand by 147 kW
- Improved energy efficiency by 24%

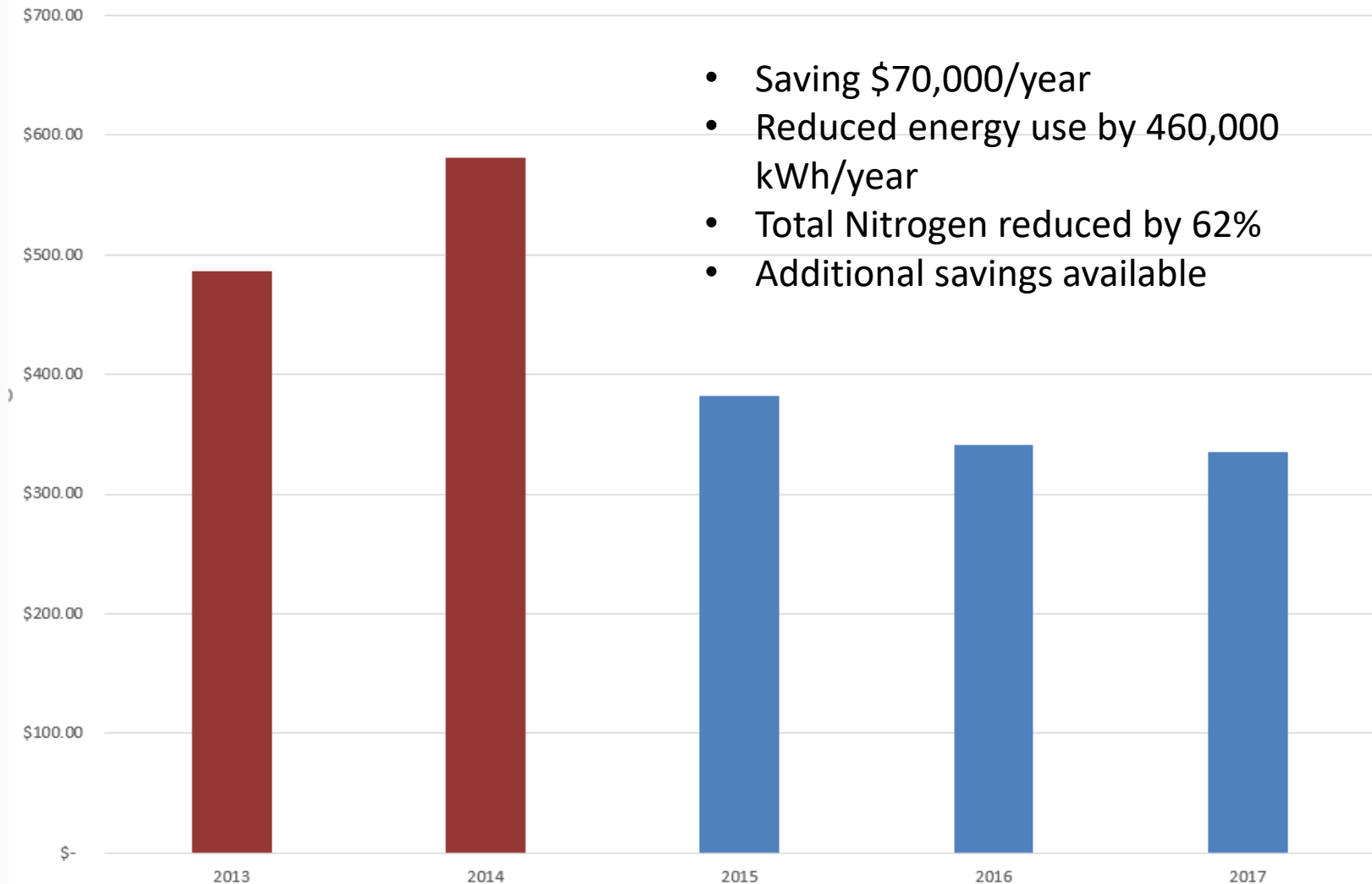
# Wetumpka, AL

---

# Wetumpka, AL

## Wetumpka, Alabama Wilako WWTP

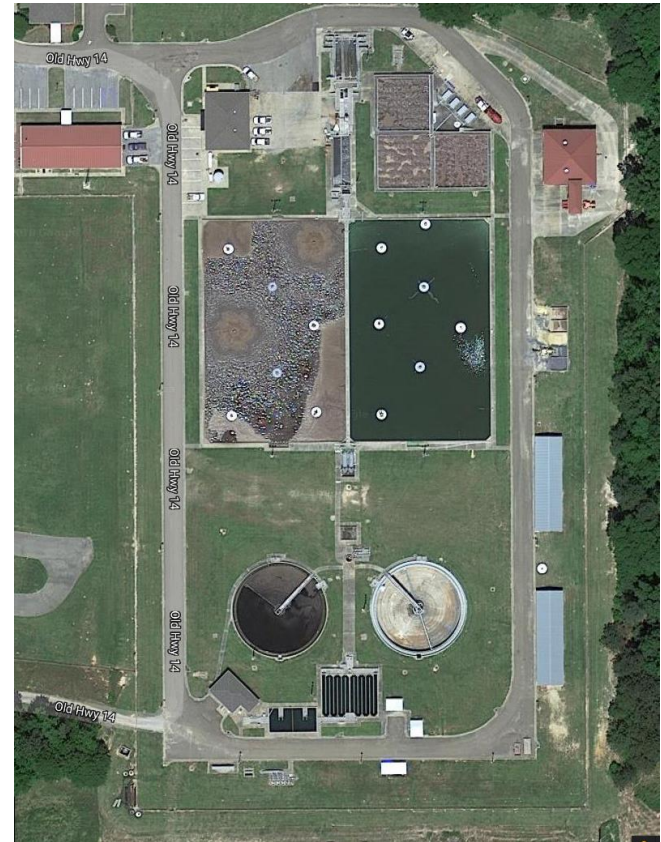
Average electricity cost per Million Gallons



Then



Now



Wetumpka, AL

# What is a kWh?

1000 kWh =



3000 miles in a Tesla Model S



# What is a kWh?

1000 kWh =



1,590 Big Mac Burgers

# What is a kWh?

1000 kWh =



What this guy eats each year  
(...by April 1<sup>st</sup>)

# Alexander City, AL

- Designed to treat domestic and industrial wastewater from a major textile manufacturer that closed during the recession.
- Eight 50-HP aerators running 24/7





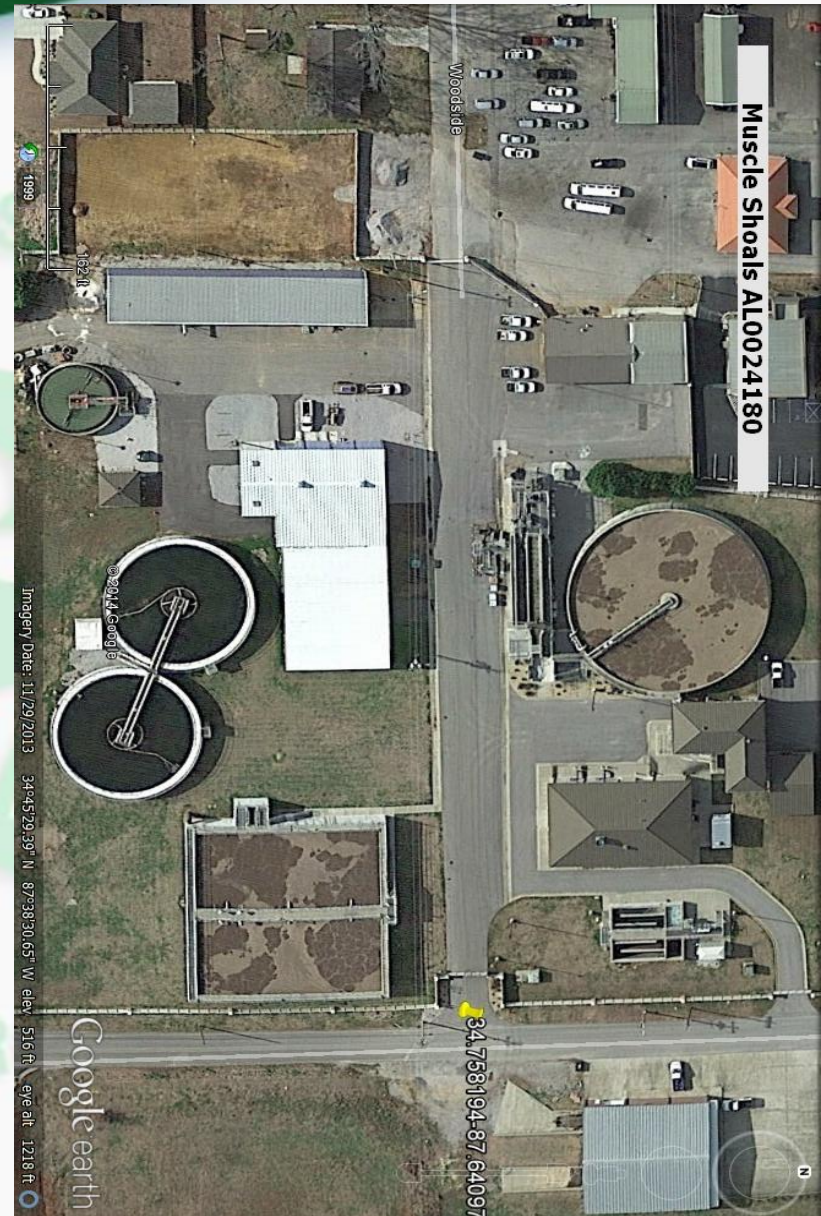
# Recommendations

- Run 4 aerators at a time, alternating every 2 hours to maintain mixing
- Plant had to install motor control relays
- Reduced total energy use by over 1,200,000 kWh/year;
- Saving over \$90k/year



# Muscle Shoals, AL

- Pop. 13,000
- 4.0 MGD design capacity
- Treats 1.3 MGD
- BOD limit = 20 mg/L
- Ammonia limit 8 mg/L
- Discharges to Pond Creek, tributary to Tennessee River



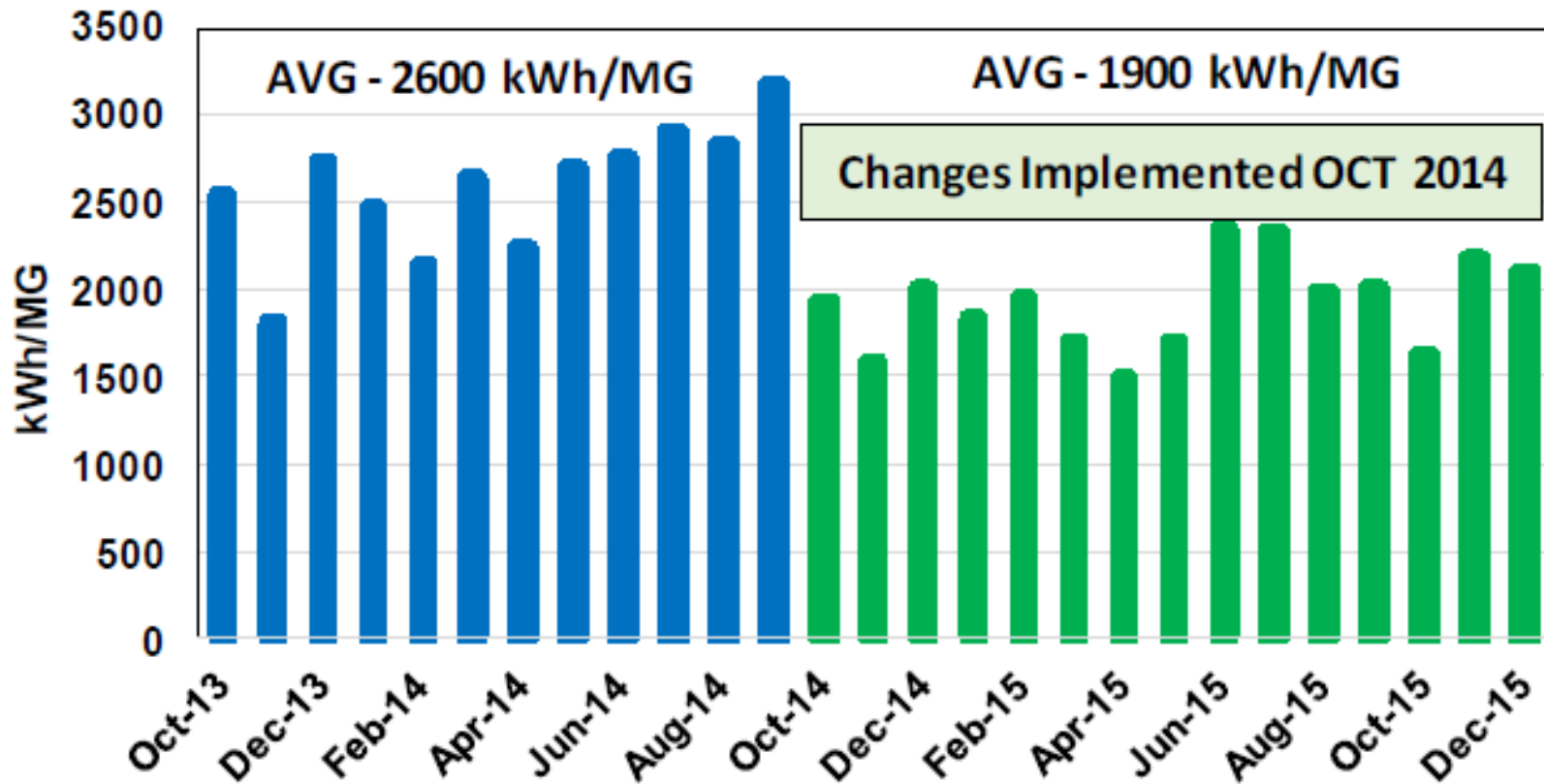


# Recommendations

- Use a smaller 150 HP aerator year-round instead of seasonally using a 250 HP aerator
- Modify bacteria concentration
- Operate one basin only
- Use on-off aeration

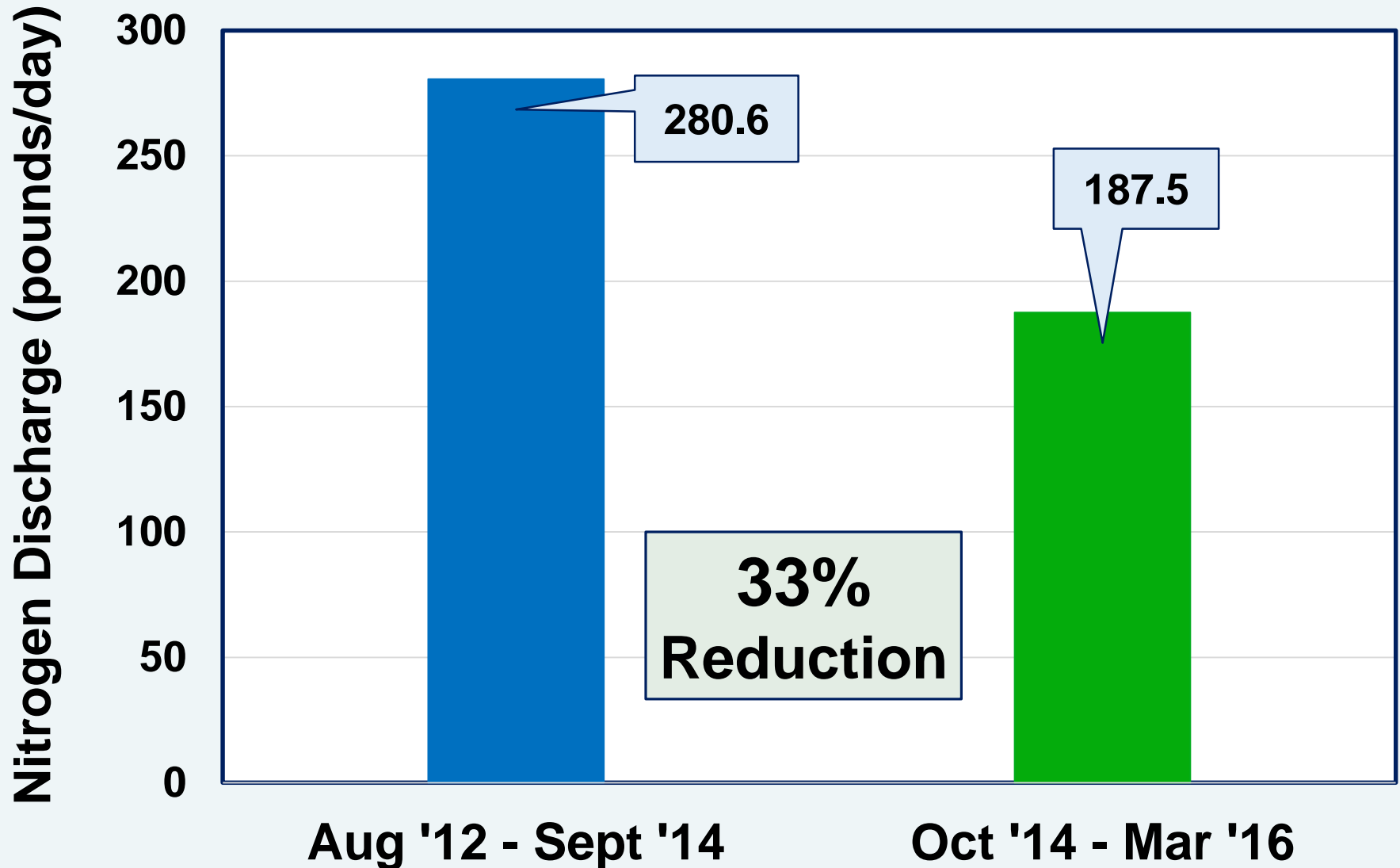


## Muscle Shoals WWTP Energy Use - kWh/MG



- 27% reduction in energy use
- 350,000 kWh/year savings
- \$11,000/year savings

# Muscle Shoals, AL WWTP Nutrient Reduction





# Resources

## Input

# Bio-Tiger Model

## Output

Current Conditions			Alternate Scenario		
Activated Sludge Input Data			Activated Sludge Input Data		
Temperature (°C)	20	1	Temperature (°C)	20	1
S <sub>0</sub> (mg/L)	200	2	S <sub>0</sub> (mg/L)	200	2
V (mil gal)	1	4	V (mil gal)	1	4
Q (mgd)	1	6	Q (mgd)	1	6
Inert VSS (mg/L)	40	8	Inert VSS (mg/L)	40	8
Oxidizable N (mg/L)	35	10	Oxidizable N (mg/L)	35	10
biomass (VSS/TSS)	0.85	12	biomass (VSS/TSS)	0.85	12
Influent TSS (mg/L)	200	14	Influent TSS (mg/L)	200	14
Inert Inorg TSS (mg/L)	20	16	Inert Inorg TSS (mg/L)	20	16
Effluent TSS (mg/L)	8	18	Effluent TSS (mg/L)	8	18
RAS TSS (mg/L)	10000	20	RAS TSS (mg/L)	10000	20
MLSS (mg/L)	3000	22	MLSS (mg/L)	3000	22
f <sub>s</sub>	0.1	24	f <sub>s</sub>	0.1	24
Y	0.6	26	Y	0.6	26
K <sub>s</sub> (mg/L)	60	28	K <sub>s</sub> (mg/L)	60	28
k <sub>2</sub> at 20°C (1/day)	0.1	30	k <sub>2</sub> at 20°C (1/day)	0.1	30
k at 20°C (1/day)	8	32	k at 20°C (1/day)	8	32
Aerator Performance Data			Aerator Performance Data		
Operating DO concentration (mg/L)	4.5	38	Operating DO concentration (mg/L)	2	40
alpha	0.84	42	alpha	0.84	42
beta	0.92	44	beta	0.92	44
SOTR, lb O <sub>2</sub> /hp-hr	2.7	46	SOTR, lb O <sub>2</sub> /hp-hr	2.7	46
Temperature (°C)	20	48	Temperature (°C)	20	48
Aeration (hp) being operated	150	50	Aeration (hp) being operated	100	50
Elevation (ft)	200	52	Elevation (ft)	200	52
Aerators operating time (hr/day)	24	54	Aerators operating time (hr/day)	24	54
Type of aerators (1, 2, or 3)	1	56	Type of aerators (1, 2, or 3)	1	56
Speed of aerators (%)	100	58	Speed of aerators (%)	85	58
Energy cost unit (\$/kWh)	0.09	60	Energy cost unit (\$/kWh)	0.09	60
Analysis			Current Conditions		
Revert to default			Alternate Scenario		
Approximate Operating Conditions			Approximate Operating Conditions		
Total average daily flow rate (mgd)	1.00	62	Total average daily flow rate (mgd)	1.00	62
Aeration volume in service (mil gal)	1.00	64	Aeration volume in service (mil gal)	1.00	64
Influent BOD5 concentration (mg/L)	200	66	Influent BOD5 concentration (mg/L)	200	66
Influent BOD5 mass loading (lb/day)	1,668	68	Influent BOD5 mass loading (lb/day)	1,668	68
Sec wv Chld N load (lb/day)	292	70	Sec wv Chld N load (lb/day)	292	70
Sec wv TSS load (lb/day)	1,668	72	Sec wv TSS load (lb/day)	1,668	72
F/M ratio	0.089	74	F/M ratio	0.089	74
Solids Retention Time (day)	28.0	76	Solids Retention Time (day)	28.0	76
MLSS (mg/L)	3,000	78	MLSS (mg/L)	3,000	78
MLVSS (mg/L)	2,242	80	MLVSS (mg/L)	2,242	80
TSS Sludge Production (lb/day)	827	82	TSS Sludge Production (lb/day)	827	82
TSS in activated sludge effluent (lb/day)	66.7	84	TSS in activated sludge effluent (lb/day)	66.7	84
Total Oxygen Requirements (lb/day)	3,121	86	Total Oxygen Requirements (lb/day)	3,121	86
Total Oxygen Req'd w/Denit. (lb/day)	2,687	88	Total Oxygen Req'd w/Denit. (lb/day)	2,687	88
Total oxygen supplied (lb/day)	3,394	90	Total oxygen supplied (lb/day)	3,185	90
Mixing intensity in the reactor (hp/ml gal)	150	92	Mixing intensity in the reactor (hp/ml gal)	85	92
RAS flow rate (mgd)	0.43	94	RAS flow rate (mgd)	0.43	94
RAS recycle percentage (%)	42.9	96	RAS recycle percentage (%)	42.9	96
WAS flow rate (mgd)	0.010	98	WAS flow rate (mgd)	0.010	98
RAS TSS concentration (mg/L)	10,000	100	RAS TSS concentration (mg/L)	10,000	100
Total sludge production (lb/day)	894	102	Total sludge production (lb/day)	894	102
Reactor Detention Time (hr)	24.0	104	Reactor Detention Time (hr)	24.0	104
VOLR (lb BOD/(thou cu ft-day))	12.48	106	VOLR (lb BOD/(thou cu ft-day))	12.48	106
Effluent CBOD5 (mg/L)	4.0	108	Effluent CBOD5 (mg/L)	4.0	108
Effluent TSS (mg/L)	8.0	110	Effluent TSS (mg/L)	8.0	110
Effluent Ammonia-N (mg/L)	0.38	112	Effluent Ammonia-N (mg/L)	0.38	112
Effluent NO <sub>3</sub> -N (mg/L)	26.0	114	Effluent NO <sub>3</sub> -N (mg/L)	26.0	114
Effluent NO <sub>3</sub> -N w/denit (mg/L)	7.8	116	Effluent NO <sub>3</sub> -N w/denit (mg/L)	7.8	116
Actual Aerator Performance			Actual Aerator Performance		
Field OTR (lb O <sub>2</sub> /hp-hr)	0.94	118	Field OTR (lb O <sub>2</sub> /hp-hr)	1.56	118
Aerator energy use (kWh/month)	70,200	120	Aerator energy use (kWh/month)	39,780	120
Energy cost (\$/month)	6,318	122	Energy cost (\$/month)	3,580	122
Cost savings vs. current conditions (\$/month)			2,738		

- Calculates oxygen demand based on process data
- User can develop equipment scenarios to match supply to demand
- Tool will estimate projected energy and cost savings, as well as nitrogen removal
- Freely available. Contact [held.brendan@epa.gov](mailto:held.brendan@epa.gov) for a copy and a tutorial.

# Bio-Tiger for Activated Sludge



# Pump System Assessment Tool

## What is it?

- Free tool downloadable from Department of Energy
- Uses flow rate, pressure, electrical measurements

- Snapshot of pump efficiency
- Compares efficiency to available pump/motor systems
- Estimates savings based on that comparison

**Pumping System Assessment Tool**

File Tools Help

PSAT 2008

**Condition A**

End suction ANSI/API

Pump rpm: 755

Drive: Direct drive

Units: gpm, ft. hp

Kinematic viscosity (cS): 1.00

Specific gravity: 1.000

# stages: 1

Fixed specific speed? YES

Line freq: 60 Hz

HP: 350

Motor rpm: 890

Eff. class: Specified (below)

FL efficiency, %: 95.4

Voltage: 460

Estimate FLA

Full-load amps: 433.0

Size margin, %: 0

Operating fraction: 1.000

\$/kwhr: 0.0800

Flow rate, gpm: 12292

Head tool: Head, ft: 62.5

Load estim. method: Power

Motor kW: 148.0

Voltage: 460

Retrieve defaults Set defaults Copy A to B Background information System curve tool: select below

**Condition B**

End suction ANSI/API

Pump rpm: 760

Drive: Direct drive

Units: gpm, ft. hp

Kinematic viscosity (cS): 1.00

Specific gravity: 1.000

# stages: 1

Fixed specific speed? YES

Line freq: 60 Hz

HP: 350

Motor rpm: 890

Eff. class: Specified (below)

FL efficiency, %: 95.4

Voltage: 460

Estimate FLA

Full-load amps: 433.0

Size margin, %: 0

Operating fraction: 1.000

\$/kwhr: 0.0800

Flow rate, gpm: 12847

Head tool: Head, ft: 51.2

Load estim. method: Power

Motor kW: 154.0

Voltage: 460

Retrieve defaults Set defaults Copy B to A Background information STOP

**Comparison Table**

	Existing	Optimal	Units	Existing	Optimal	Units
Pump efficiency	86.6	90.5	%	84.7	90.3	%
Motor rated power	350	200	hp	350	200	hp
Motor shaft power	188.2	180.1	hp	196.0	183.8	hp
Pump shaft power	188.2	180.1	hp	196.0	183.8	hp
Motor efficiency	94.9	94.6	%	94.9	94.6	%
Motor power factor	68.1	77.7	%	69.1	78.0	%
Motor current	272.8	229.6	amps	279.8	233.4	amps
Motor power	148.0	142.1	kW	154.0	145.0	kW
Annual energy	1296.5	1244.8	MWh	1349.0	1270.0	MWh
Annual cost	103.7	99.6	\$1000	107.9	101.6	\$1000

Annual savings potential, \$1,000: 4.1

Optimization rating, %: 96.0

94.1

**Log file controls:**

Create new log Add to existing log

Retrieve log entry Delete log entry

**Summary file controls:**

Create new summary file

Existing summary files: CREATE NEW

**Condition A Notes**

Facility: KUB System: Intermediate System Date: 30 July 2015

Application: Pump 1

General comments: Assumes clear well at 831.3 ft elevation

Evaluator: DAC

**Condition B Notes**

Facility: KUB System: Intermediate System Date: 30 July 2015

Application: Pump 4

General comments: Assumes clear well at 831.3 ft elevation

Evaluator: DAC



# Pump System Assessment Tool

## Who does it?

- TVA customers can get a PSAT analysis through Comprehensive Services – contact local power company to request
- DOE has Industrial Assessment Centers
  - Must have annual energy bill >\$100,000
  - Must be ~150 miles from Lexington
- DOE-certified PSAT qualified specialists (Google-able)

# Incentive Programs

## TVA Customers:

- Comprehensive services – evaluate pump & blower efficiency, PSAT analysis
- Energy Right Solutions – pays lesser of 70% of project cost or \$0.10/kWh saved during first year
  - Need to apply in advance of project work
  - Incentive money can run out over course of FY
- EnerNOC Demand response – pays you to shut down during peak periods. No penalties.

## Others:

- DSIRE – Database of Incentives for Renewables & Efficiency. Searchable by ZIP code.
- Call your local power company

# Key Points

1. There's money to be saved – and it doesn't have to cost you much
2. Management has a BIG role
3. Start small – what do you pay for?
4. You're not in it alone



# Contact Information

Brendan Held

[held.brendan@epa.gov](mailto:held.brendan@epa.gov)

404-562-8018